## FACTOR OF THERMODIFFUSION OF BINARY MIXTURES CONTAINING ALCOHOL VAPOR

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Thermodiffusion separation of the binary mixtures of argon with an ethanol, n-propanol, and iso-propanol vapor and the binary mixtures of ethanol with an n-propanol and iso-propanol vapor has been measured in the temperature range 331–347 K by the two-flask method and the thermodiffusion factor has been determined. The experimental values of the thermodiffusion factor have been compared to the results of calculation according to the Chapman–Enskog theory.

Investigation of the temperature dependence of the factor of thermodiffusion of mixtures containing alcohol vapor is of interest from the viewpoint of both obtaining information on intermolecular interactions of substances and using experimental data directly for practical purposes (calculations of technological processes) and scientific developments. In particular, the values of  $\alpha_T$  of vapor mixtures are required for determination of the critical supersaturation in investigating the process of volume condensation of the vapor [1].

The results of measurements of the factor of thermodiffusion of the binary mixtures of argon with the vapor of ethyl (CH<sub>3</sub>CH<sub>2</sub>OH), *n*-propyl (CH<sub>3</sub>CH<sub>2</sub>CH<sub>2</sub>OH), and *iso*-propyl ((CH<sub>3</sub>)<sub>2</sub>CHOH) alcohols that were carried out by us in the temperature range 279.5–325.0 K by the two-flask method have been given in [2]. The mixtures with a low concentration of the alcohol vapor ( $x_2 = 0.01$ , 0.03, and 0.05) were investigated with the aim of studying nucleation in the supersaturated vapor by the diffusion-chamber method [1].

The present work is a continuation of investigations of the thermodiffusion factor of mixtures containing alcohol vapor. By using the two-flask method [3], here we have extended the temperature range of determination of  $\alpha_T$  of the Ar-CH<sub>3</sub>CH<sub>2</sub>OH, Ar-CH<sub>3</sub>CH<sub>2</sub>CH<sub>2</sub>OH, and Ar-(CH<sub>3</sub>)<sub>2</sub>CHOH mixtures with the aim of approaching diffusion-chamber conditions as close as possible. Measurements of the thermodiffusion separation of mixtures of the same composition as those in [2] were carried out at a constant temperature of the cold volume of a thermodiffuser  $T_c = 295$  K and with variation of the hot-volume temperature  $T_h$  from 373 to 413 K. Furthermore, in this work, we have obtained, by the same method, data on the factor of thermodiffusion of the binary mixtures of the vapor of ethyl alcohol with the vapor of *n*-propyl and *iso*-propyl alcohols at the same temperatures  $T_c$  and  $T_h$ . The molar concentration of the heavy-component vapor in the mixture was equal to  $x_2 = 0.3$ , 0.5, and 0.7 at a total pressure of the mixture in the thermodiffuser of ~0.01 \cdot 10^5 Pa.

The binary mixtures were composed at room temperature according to the partial-pressure method. Chemically pure alcohols and pure (A grade) argon (argon content no less than 0.9999) were used as the components. The concentration of the mixture after its separation was analyzed by the katharometric method.

The value of the factor of thermodiffusion  $\alpha_T$  of the binary systems was determined from the relation [4]

$$\alpha_T = \frac{S}{x_1 x_2 \ln (T_{\rm h}/T_{\rm c})},\tag{1}$$

where  $x_2 = 1 - x_1$  and S is the measured value of the thermodiffusion separation of the mixture.

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Fig. 1. Factor of thermodiffusion of the alcohol-vapor mixtures ethanol–*n*-propanol (a) and ethanol–*iso*-propanol (b) vs. temperature. The experimental data (curves 1–3) and the results of calculation by the Kihara method (curves 4–6) have been obtained for the following concentrations of the alcohol vapor: 1 and 4)  $x_2 = 0.7$ ; 2 and 5) 0.5; 3 and 6) 0.3. *T*, K.



Fig. 2. Factor of thermodiffusion of the vapor-gas mixtures argon–ethanol (a), argon–*n*-propanol (b), and argon–*iso*-propanol (c) vs. temperature. The experimental data (curves 1 and 3) and the results of calculation by the Kihara method (curves 4–6) have been obtained for the following concentrations of the alcohol vapor: 1 and 4)  $x_2 = 0.01$ ; 2 and 5) 0.03; 3 and 6) 0.05. *T*, K.

The averaged values of  $\alpha_T$  were obtained from the results of no less than three experiments for each composition of the mixtures investigated. The error of the experimental data of  $\alpha_T$  was estimated at 5–8% for a confidence level of 0.95.

The values of  $\alpha_T$  were referred to the average temperature determined by the Braun formula [5]:

$$T = \frac{T_{\rm h} T_{\rm c}}{T_{\rm h} - T_{\rm c}} \ln \frac{T_{\rm h}}{T_{\rm c}}.$$
(2)

Figure 1 shows the experimental dependence of  $\alpha_T$  of the binary mixtures of the alcohol vapor on temperature for T = 330.9-347.4 K. Figure 2 gives the experimental values of the thermodiffusion factor of the mixtures of argon with the alcohol vapor, obtained by us in [2] and in the present work, at temperatures T = 279.5-347.4 K.

Mixture	<i>x</i> <sub>2</sub>	$b_1$ ·10	$b_2 \cdot 10^3$	$b_{3} \cdot 10^{7}$	<i>Т</i> , К
	0.7	0.1389	-0.2219	4.089	330—350
CH <sub>3</sub> CH <sub>2</sub> OH—CH <sub>3</sub> CH <sub>2</sub> CH <sub>2</sub> OH	0.5	0.3259	0.3304	5.608	330—350
	0.3	0.5181	0.1525	-1.350	330—350
	0.7	0.4427	0.1148	0.624	330—350
CH <sub>3</sub> CH <sub>2</sub> OH—(CH <sub>3</sub> ) <sub>2</sub> CHOH	0.5	1.4050	0.9641	15.055	330—350
	0.3	0.2207	0.0644	2.598	330—350
	0.01		1.5803	—19.634	280—350
Ar—CH <sub>3</sub> CH <sub>2</sub> OH	0.03	0.9214	0.8753	9.0026	280—350
	0.05	0.3790	0.4676		280—350
	0.01	0.8925	0.4382	7.9944	280—350
Ar—CH <sub>3</sub> CH <sub>2</sub> CH <sub>2</sub> OH	0.03	0.2879	0.04855	13.274	280—350
	0.05	0.7650	0.6407	23.579	280—350
	0.01		1.4356		280—350
Ar—(CH <sub>3</sub> ) <sub>2</sub> CHOH	0.03	0.8925	0.4213	7.8813	280—350
	0.05	—1.7129	0.9500	—1.3471	280—350

TABLE 1. Coefficients  $b_k$  of the Polynomial (3) Approximating the Dependence of the Experimental Values of  $\alpha_T$  of the Mixtures on Temperature

TABLE 2. Force Parameters of the Potential (12-6-3)

Component of the mixture	ε/ <i>k</i> , Κ	σ, nm	δ
Ar	124.0	0.3418	—
CH <sub>3</sub> CH <sub>2</sub> OH	387.2	0.4821	0.24
CH <sub>3</sub> CH <sub>2</sub> CH <sub>2</sub> OH	402.5	0.5241	0.18
(CH <sub>3</sub> ) <sub>2</sub> CHOH	387.0	0.5290	0.18

The experimental values of the thermodiffusion factor were processed by the least-squares method. Table 1 gives the coefficients of the polynomial

$$\alpha_T = \sum_{k=1}^{n} b_k T^{k-1} , \qquad (3)$$

approximating the experimental dependences of  $\alpha_T$  of the investigated mixtures of the alcohol vapor and the vapor-gas mixtures on temperature.

Figures 1 and 2 also give results of the calculation of  $\alpha_T$  by the Kihara method of a rigorous molecular-kinetic theory. For the mixtures consisting of polar components (Fig. 1) or containing a polar component (Fig. 2), the thermodiffusion factor was calculated using the potential (12-6-3). For argon we used the potential parameters [5] (Table 2) obtained from the data on viscosity, whereas for the alcohol vapor (Table 2) we used the parameters calculated from the relations [5, 6]:

$$\epsilon/k = 0.75 T_{\rm cr}, \ \sigma = (0.013698 T_{\rm cr}/p_{\rm cr})^{1/3}, \ \delta = \mu^2/(2\epsilon\sigma^3),$$
 (4)

where  $\varepsilon$  is expressed in J,  $T_{cr}$  is expressed in K,  $\sigma$  is expressed in atm, and  $\mu$  is expressed in D (1 D =  $3.1623 \cdot 10^{-25}$  N<sup>1/2</sup>·m<sup>2</sup>). The data on the critical parameters and on the dipole moments of the alcohols were taken from [7, 8].

As is seen from the figures, the disagreement between the results of experiment and those of calculation is quite considerable for all the mixtures investigated, i.e., theoretical data are capable of describing the experimental dependence  $\alpha_T(T)$  only qualitatively. It is noteworthy that the preliminary calculation of this dependence using the force

parameters of the potential (12-6-3) (these parameters were obtained in [9] for the alcohol vapor from the data on viscosity) has shown an even larger disagreement with experimental values. Therefore, we may state that only experiment can be used at present as quite a reliable source of obtaining data on the thermodiffusion factor of mixtures containing polar components: the vapor of ethanol, *n*-propanol, and *iso*-propanol.

## NOTATION

 $b_k$ , polynomial coefficients; k, Boltzmann constant; p, pressure; S, separation of the starting mixture in the thermodulfuser; T, temperature; x, molar concentration of the components of the starting mixture;  $\alpha_T$ , thermodiffusion factor;  $\delta$ ,  $\varepsilon/k$ , and  $\sigma$ , force parameters of the potential (12-6-3);  $\mu$ , dipole moment. Subscripts: c and h, cold and hot volumes of the thermodiffuser; 1 and 2, first (light) and second (heavy) components of the binary mixtures investigated experimentally; cr, critical values of temperature and pressure.

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